

Appl. No. 09/643,755
Amtd. Dated
Reply to Office action of December 16, 2003

REMARKS/ARGUMENTS

By the present amendment, claims 1, 17, 21 and 22 have been amended, claims 18-20 have been deleted and a new claim 21 has been added. The amendments to the claims have been made without prejudice and without acquiescing to any of the Examiner's objections. Applicant reserves the right to pursue any of the deleted subject matter in a further continuation, continuation-in-part or divisional application. The amendment does not contain new matter and its entry is respectfully requested.

The Official Action dated December 15, 2003 has been carefully considered. It is believed that the amended specification and the following comments represent a complete response to the Examiner's rejections and place the present application in condition for allowance. Reconsideration is respectfully requested.

35 U.S.C. §102

The Examiner has objected to claims 1, 3, 5-7, 11 and 13-19 under 35 U.S.C. 102(b) as being anticipated by Willmitzer et al. (WO 92/01042).

By the present amendment, independent claims 1 and 17 have been amended in order to incorporate the subject matter of previous claim 20 which has been deleted. We note that previous claim 20 was not under objection and therefore amended claims 1 and 17 and the claims dependent thereon are novel. In particular, Willmitzer does not disclose the method of isolating chymosin from plant seed as described in step (d) of these claims.

Claim 1 has also been amended to remove the requirement that the seed contains at least 0.5% (w/w) chymosin as the Examiner feels the percentage yield is not a distinguishing feature of the claims over Willmitzer.

In view of the foregoing, we respectfully request that the objections to the claims under 35 U.S.C. 102 (b) be withdrawn.

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35 U.S.C. §103

The Examiner has objected to claims 1-8, 10, 11 and 13-23 under 35 USC §103(a) as being unpatentable over Willmitzer et al. and further in view of Applicant's admitted prior art.

As mentioned above, the independent method claims 1 and 17 have now been amended in order to include steps for isolating the chymosin from the plant seed. The steps involve fractionating crushed seed into an oil fraction, an aqueous fraction and a fraction comprising insoluble material and then subsequently contacting the aqueous fraction containing the chymosin with a protein binding resin. None of these steps are disclosed or suggested in Willmitzer. Further, one of skill in the art would not be motivated to include such steps having read Willmitzer for the following reasons.

First, as Willmitzer does not prepare chymosin in seed, Willmitzer does not isolate chymosin from seed. Willmitzer uses a constitutive promoter which results in the expression of chymosin in various plant parts and Willmitzer isolates the chymosin from the leaves. Second, Willmitzer does not prepare chymosin in plants containing high levels of oil. Willmitzer only works in tobacco and potato plants. Consequently, Willmitzer would provide no motivation for one of skill in the art to develop methods to isolate chymosin from oil seeds.

At the time that the invention, recombinant proteins had been prepared in oil seeds. However, the purification of recombination proteins from oil seeds was difficult due to the presence of large quantities of oil which would make the subsequent purification steps problematic. The art-recognized solution to the problem was to extract the oil using conventional hexane extraction procedures. However, the use of hexane or other organics solvents to extract proteins was not desirable due to the denaturant property of such solvents. We are enclosing a paper by Cramer et al. (*Current Topics in Microbiology and Immunology*, Vol. 240, p. 95-118, 1999) which states at page 107 that "methods of efficiently recovering proteins from the apoplastic fluid have yet to be developed".

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The problems of the prior art were solved by the present invention. In particular, the present inventors determined that chymosin could be recovered by fractionating the crushed plant seed into an oil fraction, an aqueous fraction and a fraction comprising insoluble material using an aqueous extraction protocol. Organic solvents are not required which overcomes the disadvantages of the prior art.

In view of the above, the claims of the present invention are inventive over Willmitzer as Willmitzer provides no disclosure, suggestion or motivation to isolate the chymosin from plant seeds using aqueous extraction. We do not understand the Examiner's statement on page 7 of the office action that states that "Willmitzer teaches methods of protein isolation using a protein binding resin". Respectfully, we cannot find any disclosure in Willmitzer that relates to the use of a protein binding resin.

The Examiner has also objected to claims 1-8 and 10-23 under 35 USC §103(a) as being unpatentable over Willmitzer and further in view of Adang et al. (U.S. 5,380,831).

As mentioned previously, the independent claims have now been amended in order to include steps for isolating the chymosin from the seed. The claims are clearly inventive over Willmitzer for the reasons stated above. The deficiencies in Willmitzer are in no way remedied by Adang as Adang is not concerned with methods of preparing chymosin in plant seeds and with methods of isolating the chymosin from the plant seeds.

In view of the foregoing, we respectfully request that all of the objections to the claims under 35 U.S.C. §103(a) be withdrawn.

The Commissioner is hereby authorized to charge any deficiency in fees (including any claim fees) or credit any overpayment to our Deposit Account No. 02-2095.

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In view of the foregoing, we submit that the application is in order for allowance and an early indication to that effect would be greatly appreciated.

Respectfully submitted,

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Attachments

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Transgenic Plants for Therapeutic Proteins: Linking Upstream and Downstream Strategies

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1. Introduction

With the new knowledge generated through the Human Genome Project and related biomedical research comes a potential revolution in drug development strategies. One of the most direct applications of this knowledge will be highly specialized recombinant protein-based therapeutics. Recombinant drugs such as human erythropoietin (rEPO), tissue plasminogen activator (tPA), and Cetuximab (afibrotucostatida) are currently on the market and many other recombinant proteins are in various stages of human clinical trials. Commercial production of

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Table 1. Feasibility of plant-based production of human (or other animal) proteins

Transgenic product	Plant host disease target	Fruit/leaf tissue	Starch/seed integrity	Functional activity	Reference
Human prothrombin	Blood coagulation factor V	Vicia faba	Yes	Yes (O'Doh) Not tested	Davies et al. 1997
Human serum albumin	Blood coagulation factor C	Papaya	Yes	Not tested	Singh et al. 1990
Human fibrinogen	Atherosclerosis	Tobacco	After germination	Anticoagulating activity	Chandekar et al. 1996
Oxytocin/beta-phthalide receptor antagonists	Uterine contractions	Tobacco	Yes	Yes (analogue activity)	Zurek et al. 1994
Interferon	Parvovirus	Tobacco	Yes	Yes (in vitro assay)	Gao et al. 1997
c-IL-12	Lymphoproliferation Lymphokine-activated killer cell culture	Tobacco	Yes	Yes (cytotoxic assay)	Gao et al. 1996
Human IgG	Antibody production	Nicotiana tabacum	Yes	Yes (functional assay of T-cell lysis)	Hiroo et al. 1993
Root glucuronidase	Milkose fructose	Tobacco	Yes	Not tested	Boddy et al. 1994
Riboflavin	Milkose, blood cells	Tobacco	Yes (Growth*)	Not tested	Matsuura et al. 1995
Lysosomal enzymes	Fatty disease	Tobacco	Yes	Yes (regulatory activity)	Quill et al. 1997
c-Galactosidase	Glucuronidase/Chlorhexidine resistance	Tobacco	Yes (Growth*)	Chamlin et al. 1996	
Other proteins	Neutrophilic antiphosphatidyl choline	Potato	CRIM*	Not tested	Cirigliano et al. 1997
Human	Antiphosphatidyl choline	Cannabis	Yes	Yes (hemolysis assay)	Parhamizan et al. 1995
NP1 dectinin	Antifreeze	Tobacco	CRIM*	Yes (antifreeze assay)	Gao et al. 1997
Chitosanase	Diabetes	Tobacco	CRIM*	Yes (in vitro assay)	Bax et al. 1997
Chitosanases					

*Proteins were synthesized but the plant composition may differ from those produced in bacteria.

*Detected as cross-reactive immunoreacted method by western immunoblot or ELISA.

these proteins utilizes fermentation (primarily *E. coli* and yeast) and mammalian cell systems (e.g., Chinese hamster ovary cells), the major expression system adopted by the well-established biotechnology companies. However, these expression systems have significant limitations. *Bacillus subtilis* performs the complex posttranslational modifications required for biactivity of many human proteins and bacterial endotoxins and black-field storage often leads to degradation of insoluble protein aggregates. While mammalian cell cultures perform the required protein modifications, low transgene expression levels, loss of viability of selected cell lines, and the difficulties and high expense of scaling up are often financial or severely impact cost. Thus there remains a significant opportunity for alternative expression systems that address these limitations and cost issues to contribute in the protein therapeutics market. In fact, development of more cost-effective protein bioproduction systems may be critical in translating the discoveries of genetics and modified recombinant DNA technology into available and affordable treatments and cures. Recent advances in the area of biologics include the use of genetically-modified plants and animals for bioproduction. Indeed, plants provide an effective protein factory. The fact that recombinant proteins from plant, mammalian animal and bacterial proteins are safe in clinical trials demonstrates significant promise toward commercialization of these technologies.

For any particular target protein, selection of a recombinant system will depend on the characteristics of the desired protein product, the volume needs (size of the market), and market-driven cost constraints (reviewed by Pez 1996). Transgenic plants have some remarkable features that make them particularly well suited for cost-effective bioproduction of proteins for pharmaceutical use. These include: (a) low production costs, (b) reduced time to market, (c) unlimited supply, (d) long-term protein processing, and (e) safety. Cost advantages are based not only on the low cost of biomass production, but also costs associated with research and development, equipment scale-up (e.g., imagine the infrastructure investment of tripling the capacity of one's aseptic fermentation or mammalian cell production facility compared to tripling one's acreage for plant growth), and reduced requirements for quality assurance testing for exclusion of common pathogenic agents (reviewed in Omera and Pez 1996). Plant-based strategies also have advantages in the pace at which feasibility testing can be done and R & D successes can be scaled up and brought to market. For example, a tobacco plant goes from seed to next generation seed in three months and produces up to a million seed per plant. Scaling-up to hundreds of thousands of acres is very rapid.

Many of the therapeutic proteins of interest require complex posttranslational processing and/or oligomerization for bioactivity or appropriate targeting following administration to patients. There appears to be remarkable conservation of these protein processing steps between plants and animals and that the majority of human proteins that have been produced in plants (see Table 1) show significant structural, biochemical and functional equivalence to proteins from humans or animal cell cultures. In cases where certain modification steps are lacking or differ in plants (e.g., glycan composition, discussed further below), strategies to introduce appropriate animal protein processing enzymes or modify the plant processing

machinery are greatly facilitated by the ease of plant transformation and the broad experience in transgenic approaches to modifying plant metabolism through over-expression and antisense strategies. In fact, plants may be the only system capable of efficient production of certain human proteins such as growth regulators and cell cycle inhibitors which would negatively impact either the transgenic animal or animal cell culture in which they are expressed.

Perhaps the most important advantage of plants, which is emerging in the aftermath of the recent "mad cow disease" scare, involves product safety. The biopharmaceutical industry is faced first with the possibility of product validation

and quality assurances that demonstrate purity not only from known human pathogens such as HIV but also from unknown or poorly characterized agents such as the prions responsible for bovine spongiform encephalopathy and the related Creutzfeldt-Jakob disease (Brodie and Jantzen 1996; Vaughan 1996). Plants do not serve as hosts for blood- or animal tissue-borne human pathogens. In addition, plant-based production and purification can be executed without the use of any animal-derived products. Quality purity, efficacy and quality control issues pertinent to production of any biologics must be addressed (see Miller 1997).

However, plant-based bioproduction should realize substantial savings on a human-safe and source-free production system. The list of complete human proteins and animal, viral and bacterial proteins of medical value that have been successfully expressed in plants is growing rapidly (reviewed in Green and Pez 1996). In addition to disease-benign (viruses) and antisera discussed in other chapters of this volume, transgenic plants have been used to synthesize a number of complete human proteins. Glycoproteins, growth regulators, antibiotics, carbohydrates, and lyticosomal enzymes (see Table 1). Most of these proteins appear fully functional and structurally comparable to the analogous proteins produced in animal cell cultures or in humans. Thus, plants have already passed the initial test of feasibility: they are capable of producing biopharmaceutical proteins of pharmaceutical value. In addition, the first transgenic plant-synthesized products (a tobacco-derived antibody targeting gum disease and a potato-derived edible vaccine candidate) have reached initial human trials – a significant benchmark toward commercialization. However, as we move from feasibility studies to commercial bioproduction, issues of transgene expression levels, product processing and stability, biomass and extraction scale-up, purification, and quality control become paramount. These long-term goals have inspired the development of novel transgenic expression systems that incorporate components targeting product abundance, product recovery, and regulatory acceptance into the initial transgene design. In this review, we will discuss key issues that impact the choice and utility of plant-based production systems for biopharmaceuticals. We will highlight several production strategies that stress the importance of thinking "upstream" (i.e., in genetic engineering and expression strategies with "downstream" issues of extraction, purification, and yield). These systems are designed to separate biomass production from transgene protein production and to directly manipulate the transgene tissue and subcellular localization of the product to enhance yield, protein stability, and ease of recovery and purification.

2 Plant-Based Biopharmaceutical Productivity: Issues and Answers

The majority of examples demonstrating bioproduction of potential therapeutic proteins in plants appear in Table 1. In general, model plant species that are easy to genetically engineer (e.g., *Solanum tuberosum*, *Potato*) and the "string bean" (*Phaseolus vulgaris*) have been used for the production of the particular protein of interest but

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Table 2. Transgene expression strategies and recombinant protein yields

Transgene product	Transgene	Plant host	Producer	Expression strategy	Production level (% of total protein)	Reference
Human IgG1 Human serum albumin	Protein C	Tobacco	35S	Seed, root Constitutive, leaf	1.02%	Davies et al. 1997
Cytokine/antiphotosensitizer	Ricin	Tobacco	35S	Constitutive, leaf	0.09%	Chapman et al. 1996
Thiostresemone	Tobacco	N/A	EF	Constitutive, leaf	Not reported	Zheng et al. 1994
CH-CP	Tobacco	Tobacco	35S	Constitutive, leaf	1%	Green et al. 1997
Biotinidase Lysozyme/nutrients	Tobacco	Tobacco	35S	Seed-specific Constitutive, leaf	Not reported	Gao et al. 1996
α -Glucosidase	Tobacco	N/A	Cherry/EF	12.1 mg/g biomass	Green et al. 1997	
Glucuronidase	Tobacco	MaCPA	Pod-barrel leaf tissue	1%–10%	Chen et al. 1996	
Viral or bacterial antigen <i>X. col</i> enterotoxin B Cobra toxin	Tobacco	N/A	Constitutive, leaf	Not reported	Haque et al. 1995	
Hepatitis B surf. antigen	Tobacco	35S	Constitutive, leaf	10.07%	Haque et al. 1992	
Oncovirin	Chlorrella	Chlor	Oscillin	Microtiter	10.00%	Haque et al. 1995
Antibodies	Tobacco	N/A	Constitutive, leaf	Not reported	Henry et al. 1996	
α -Trichosanthin	Tobacco	N/A	Constitutive, leaf	4%–5%	Kimura et al. 1993	
Glutamine decarboxylase	Tobacco	35S	Constitutive, seed Tissue	0.4%	Nik et al. 1997	
					0.4%	Mu et al. 1997

*Modified S38 promoter containing anti-water induction and/or tandem sequences (translational enhancers) from the tobacco etch virus or tobacco mosaic virus.

projector derived from the cauliflower mosaic virus. However, as plant biotechnology moves from demonstrating feasibility toward commercialization of protein products, many other issues come into play in selecting host species, expression strategies, target tissues, and extraction/purification protocols. These choices must take into account not only the production of the particular protein of interest but

for: Dr. David A. Parr
Subject of recovery, purity, production/purification costs, reproducibility, supply
conditionality, quality control and regulatory assessment.

2.1 Selection of Crop Species

While certain features such as low production costs and high biomass capacity are common to all plant-based expression systems, other factors may strongly influence the choice of one plant species or expression strategy over another for the production of a specific foreign protein. In selecting a particular species it is important to consider how easily it can be manipulated to produce a stable transgenic line, the tissue and subcellular compartment best suited for stable expression of the heterologous protein, and the availability of methods for the efficient harvesting and initial processing of the plant material. Included in the first consideration are factors such as the susceptibility to transformation and regeneration of white plants, germination time, and capability to controlled genetic crossing. All of these factors significantly impact upon the time and resources required for product development. Plant transformation technologies are highlighted in other chapters (Flavell and Clifton and Flavell et al., this volume) and have been recently reviewed (Leppla 1990) and are therefore not discussed in detail here. The remaining two considerations deal mainly with product biocompatibility (bioactivity, conformation, efficacy) and recovery. Because infrastructure and methods for the harvest and processing of the major crop species already exist, whatever possible these are the species of choice. The costs and subcellular compartment of expression determines product processing capabilities, stability of the product and the ease with which it can be harvested.

For crop transgenic the choice of plant to genetically engineer, and is widely used to test suitability of a specific system for the production of recombinant proteins (see Table 2). Although tobacco is considered a research crop and relatively labor intensive at least three plant species are targeting tobacco for biopharmaceutical production (Cronenwett, Corn, Hisamatsu Technologies Inc. and Pharmatech). In addition to being easily engineered, tobacco is an excellent biomass producer (in excess of 40 tons leaf fresh weight/year based on multiple mowings per season) and profits/seed producer (up to one million seeds produced per plant), thus hastening the time in which a product can be scaled up and brought to market.

Several companies are developing production strategies involving transgenic product accumulation in seeds, an organ designed to accumulate and store protein reserves (see Sect. 2.2). Companies targeting seed-based production using canola, corn or soybeans include Stem Bioscience Genetics, AgriGenics (USA), Migen International (The Netherlands), and Plantzyme (the Netherlands). Applied Phytogenics (API, Davis, CA) is using transgenic rice and barley seed, bat is producing and recovering recombinant proteins during seed germination in a process analogous to malting. Other crops being developed for biopharmaceutical protein or vaccine production include alfalfa, beans, potato, and tomato.

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2.2 Choice of Tissue

In order to obtain maximum yield, the plant species selected must concentrate biomass in the organ or tissue where the foreign protein is expressed. The diversity among different species in this respect means that a variety of organs are available including leaves, vegetative storage organs (e.g. tubers) and seeds. The biomass chosen should be compatible with the desired protein, enabling correct processing, stable denaturation and, whenever possible, efficient recovery. Many human therapeutic proteins require extensive processing for full activity, involving transport through the cellular endoplasmic reticulum system. Functional lysosomal enzymes (Cavazzini et al. 1990b) and mammalian antibodies (Müller et al. 1992) have all been produced in leaves of tobacco following transfection through the endoplasmic reticulum (ER) and Golgi complex. Human serum albumin has also been stably expressed in tobacco leaves and various tissues of potato including tubers (Gutierrez et al. 1990), although the precise folding and functionality of the protein was not established. In the above examples the recombinant proteins were either specifically targeted to and directed in the apoplastic, or presented to, locate there as a result of the default pathway of the plant endomembrane system. Degradation into the extracellular apoplast may contribute to the stability of foreign proteins by removing them from the more hydrolytic intracellular environment (Perez et al. 1992).

Expression and accumulation of foreign proteins in seeds may be achieved through co-expression of a viral vector sub-cellular storage organelle. As a natural storage organ, seeds possess attributes such as high protein content and a low nucleic acid-to-protein ratio and contain the single, then particularly attractive as a product, production vehicles - the ribosomes - less cytoplasm (Van der Valk et al. 1987), and the large, autogenous protein, albumin (Panahie et al. 1995), have both been included in seeds of *Bracon hebetor* following injection of protein bodies and oil bodies respectively. Proteins can also be sequestered to the apoplast of seeds. However, the economy of apoplastic proteins from seeds may be more difficult than from some of the vegetative organs mentioned above, owing to the deserved state of intact tissue vulnerability. On the other hand, this advanced state of dayordination also confers enhanced stability, although seeds to be stored for periods of several years without any appreciable degradation of protein or loss of activity (e.g. see Perez et al. 1992). The greater stability resulting from the separation of protein production and purification represents a distinct advantage of seeds over most other organs for which more immediate processing is often required.

2.3 Expression Strategies

Choice of promoter, which mediates the timing, tissue-specificity, and level of transgene expression, is a key determinant of transgenic product yields and recovery strategies (see review by Cai and Cowan 1995). As shown in Table 2, many of the human (or other animal) proteins expressed in plants have used native or enhanced

versions of the 35S promoter derived from the cauliflower mosaic virus to drive "constitutive" transgene expression, and it remains the most widely used promoter in plant biology for over-expression of plant proteins or inhibitors via antisense strategies. The 35S promoter is active in most plant tissues (Bayer et al. 1989; Raskin et al. 1989) and, especially in its modified form (Klein et al. 1993; Cox-Smerdon and French 1990) can drive quite high levels of protein production. Although most of the human proteins produced using the 35S promoter (Table 2) showed accumulation levels below 0.1% of soluble protein, several transgenic products (antibodies, antibodies) have been expressed at levels of 2%-5% of extractable protein. The 35S promoter is quite active during seed development and has been used in production systems targeting recovery of recombinant proteins from seed. However, the 35S promoter (and constitutive expression in general) has significant limitations when commercial bioproduction in nonseed tissues is the goal. Production is inextricably tied to high levels of may negatively impact yield or overall health of the plant. High constitutive expression is sometimes associated with co-expression of gene silencing (Tavare 1997) resulting in little or no transgene product accumulation. For proteins that are not highly stable, constitutive expression can lead to wasteful synthesis, degradation cycles, and/or particular difficulties for pharmaceutical application. Accumulation of our final product with inedible degradation products. In addition, the 35S is not highly active in many ordinary tissues (e.g., vegetative roots and fully expanded leaves) so that the full potential of human cannot be utilized. Use of inducible promoters or promoters that have low levels of tissue- or organ-specificity avoids many of these limitations and appears to be the strategy of choice for most companies targeting plant-based production of therapeutic proteins.

Coxon et al. (1991) have developed a postharvest expression system that uses an inducible promoter, termed the MeGA™ promoter (Coxon and Winklerová 1990). This promoter is induced by a defense-related gene such that it is usually inactive during normal growth and development but shows rapid and strong gene activation in response to mechanical stress (wounding-induced, etc.) and chemical agent (ethylene) or a variety of defense substances. Thus, the recognition problem is circumvented in tobacco leaves in the field (or greenhouse). Plants can be harvested and stored for weeks in a cold room. Recombinant protein production is also induced as above in the laboratory. Cell壁 and newly synthesized protein recovered 5-20% later. Recovery survival depends on both the speed and intensity with which a plant can activate its defense; we find the MeGA™ promoter highly effective in driving high levels of inducible expression in all tissues of the plant, including fully expanded leaves. The postharvest expression strategy has several advantages for pharmaceutical production. Biomass production is both temporally and spatially separated from recombinant product production minimizing two impact of (a) environmental factors on protein yield and quality and (b) possible deleterious effects of transgene expression or foreign protein accumulation on plant growth and development. All recovered protein is nearly synthesized. In addition, the timing of protein extraction can be adjusted based on the stability of the particular gene product to optimize yield of fully active polypeptides.

tides. For products requiring activation of multiple genes (e.g., multiple subunits, or target proteins that require specialized protein-modifying enzymes), co-expression assures coordinated synthesis. In theory, the postharvest system could also permit further manipulation of the protein synthesis and processing machinery through addition of specific chemicals to the induction medium (e.g., inhibitors of key protein modifying steps), although this could add significant expense to commercial scale bioproduction.

Bioproduction strategies involving developmental period, or viability, regeneration (e.g., Bioscience's Clematis System) are also designed to limit recombinant protein production to a discrete period. With the Clematis system, the Viability-tolerant tobacco is held green to an appropriate age, inoculated with genetically modified virus, and harvested 2-3 weeks later for recombinant protein extraction (Quintal 1997). Within this period, the plants die, reach high levels leading to significant transcriptase product accumulation. Using this system, Bioscience actually have attained very high product yield (recombinant protein representing greater than 10% of total soluble protein) but have progressed to the point of large scale seed production and pilot plant construction. Applied Biologics utilizes a gene knockout-specific promoter to direct transgene expression. Recombinant protein is produced under controlled conditions following induction and initiation of germination of transgenic seed, a production scheme analogous to today's existing bioproduction strategies involving seed-based accumulation of recombinant proteins. One salient advantage of discrete bioproduction periods is avoidance of radioactive activity from the half-life plant product. A large number of seed-specific promoters, often derived from genes encoding seed storage protein, are available for both monocot and dicot plants. Depending on the recovery strategy (see below) and the characteristics of the protein (protein, proteins specific for embryo- versus endosperm-specific expression) can be selected.

2.4 Posttranslational Processing

In comparison with bacterial systems production, heteroproduction of human proteins for pharmaceutical applications is particularly challenging due to the rigorous requirements with respect to purity, reproducibility, efficacy, and biocompatibility. Many of the proteins will, greatest promise as therapeutics require complex post-translational modifications and/or assembly. The striking fidelity with which plants appear to recognize and correctly act upon most of the processing signals encrypted within mammalian polypeptides indicates a high degree of conservation in protein processing machinery between plants and animals. Conserved processes include endomembrane targeting, signal peptide cleavage, protein folding and oligomerization, disulfide bond formation (although precise cysteine-cysteine bonding patterns have not been directly determined), asparagine-linked glycosylation, selective refolding in the ER and Golgi, and C-terminal isopropylation. We have also noted internal proteolytic processing events in several human proteins expressed in tobacco that appear to mimic processing that occurs in mammalian cells

although the protein terminal of the proteins have not yet been determined (Oliver et al., unpublished data).

However, clear differences in protein processing, most notably in oligosaccharide processing do exist between plants and animals. The glycan majority of mammalian glycoprotein functions is protein folding and assembly, subcellular targeting, cell or tissue-specific delivery within the body, protein half-life, and clearance from the bloodstream (Vance 1995). Tissue changes in glycan composition or arrangement are likely to affect activity or pharmacokinetics (Carrasco et al. 1996; Lotz 1992). Plant modified glycans do not contain terminal sialic acid residues or mannose-6-phosphate and contain other sugar or sugar linkages not found in mammalian glycoproteins. The plant unique sialic acid signature (N-X-S/T) is recognized within the ER (or addition of the Mannose-N-linked Glycan complex, identical to plant and animal). However, plant processes these N-linked glycans to distinct complex forms at the glycosome. In plants, through the Golgi, the sialic acid is present at the terminal sugar on many human glycoconjugates and appears to function in sensitivity and rates of clearance for some serum fractions (Gaudelli et al. 1991). The combination of this changed sugar residue into protein glycans has not been demonstrated in plants (Perry et al. 1996). In addition, plants do not phosphorylate high-mannose glycans – in mammals, the mannose-6-phosphate serves as a signal to target soluble glycoproteins to lysosomes. Finally, many complex plant glycans contain either fucose or xylose residues with linkages that do not occur in humans. Plant-synthesized glycoproteins displaying these sugar linkages appear highly immunogenic when injected into mammals (Carrasco and Fava 1996). Interestingly, an *Anabiosperma* mutant defective in *N*-acetylgalactosaminy-l-transferase-I has been identified in which all N-linked glycans are in the high-mannose form (van Schuppen et al. 1993). This report suggests that processing of glycans to complex formats is not critical for plant viability or development (in contrast to animals). Thus, plants can be altered to produce nonimmunogenic glycans. Variations in glycan composition is not unique to plant-based recombinant systems – yeast, bacterial, insect, cell, transgenic animal, milk and even mammalian cell cultures often generate glycans that are heterogeneous or differ significantly from the native configuration for particular human proteins (reviewed in Jevons et al. 1996). It is clear that additional research is required for effective bioproduction of human glycoproteins in plants (discussed further for lysosomal proteins in Sect. 3). Genetic engineering strategies to modify the glycan processing machinery of plants or *in vivo* enzymatic modification of the purified recombinant protein should enable commercialization of plant-synthesized glycoproteins for pharmaceutical applications.

Because plants are relatively easy to genetically engineer, genetic strategies to specifically alter protein processing by either antibiotic to block endogenous enzymes or addition of genes encoding novel processing activities are highly feasible. The recent cloning of plant genes encoding enzymes involved in Golgi-localized glycan processing opens up opportunities to modify the complex glycans produced in plants. Processes other than glycosylation can also be modified. We are interested in testing whether plants can be engineered to produce the complex serum proteins involved in the coagulation/anticoagulation cascade (Crosser

et al. 1996; Wenzelovova et al. 1997). Plants are unlikely to perform the highly specialized carbohydrate portion of the amino-terminal glucanases required for hydrolysis of several of these enzymes (firsts C, chitinase, chitoglucanase, etc.). We are currently investigating a human apGNA (or the vitamin K dependent prothrombinase activator) for its ability to perform the necessary modifications for this class of proteins in tobacco (Crumm, Chapman, et al. (unpublished data)). While these experiments are in very early stages, the concept of engineering elite plant lines for specialized protein processing for pharmaceutical production seems highly feasible.

2.5 Recovery Strategies

To capitalize on the advantages of plant-based systems in upstream production, it is necessary that downstream purification of the recombinant product be accomplished economically. Current and inefficient purification schemes can contribute significantly to overall costs and result in lower yields so that commercial production is no longer viable. In some cases, such as in the production of industrial enzymes, downstream costs can be reduced or even eliminated when a high degree of product purity is not required. A good example of this is the production of phytase in seeds. The enzyme phytase may be used to enhance the nutritional quality of seed meal by breaking down the phytate present in the meal and thereby increasing the availability of phosphate to monogastric animals. This may be conveniently achieved through expressing the phytase enzyme in seeds and adding milled transgenic seed to a standard feed meal preparation (Penn et al. 1993; Vlietveld and Penn 1990). Unfortunately, this strategy is not applicable to many proteins, particularly pharmaceutical proteins, that require chromatography to purify homogeneously. For these products simple and efficient methods of downstream purification must be developed.

2.5.1 Affinity Tag-Based Purification

One approach to the purification of recombinant proteins is through the use of affinity tags. This can be accomplished through the creation of a fusion between the protein of interest and another protein or peptide that exhibits affinity for a specific ligand. The fusion protein is then recovered by binding to the ligand immobilized onto a support matrix. The high selectivity possible with affinity separation often enables a substantial degree of purification to be achieved in a single step. A number of these affinity tags have been developed for use in microbial systems. Different types of ligand pairs have been exploited for this purpose including maltose binding protein-amylose, histidine residues-metal ions and protein A- IgG. A similar approach may be useful for the purification of recombinant proteins synthesized in plants. The efficacy of this method in plants has been demonstrated in a small scale purification of a human glucocerebrosidase-FLAG epitope fusion produced in tobacco (Chameau et al. 1996). Here, the fusion protein was recovered using an anti-FLAG antibody affinity matrix and used for bio-

chemical analogs on activity and posttranslational modifications. However, because the long-term application is as a replacement enzyme therapeutic for Gaucher patients, the presence of the "nonhuman" residues is undesirable and is not desirable for scale-up. For some proteins and production strategies, the addition of non-native amino acids can be removed from the native protein following purification. However, as with any strategy involving cleavage or removal of fusion proteins, the addition of the signal peptide and/or endopeptidase to the recombinant protein could be problematic due to its contribution to the formation of inclusion bodies.

2.5.2. Coexpression strategy

Another method of simplifying the purification of recombinant proteins is through coexpression of the protein. This can be achieved using either signal peptides or whole protein fusions in which the protein is fused to a specific cellular location. In this case, purification of the desired protein is facilitated by virtue of its physical association with the oil bodies. In oil seedbeds, the oil bodies are spherical inclusions containing a variety of proteins. A variety of fusion strategies have been employed for the induction of foreign proteins in plant tissues. These include co-expression of oil and tobacco mosaic virus (TMV) and bipartite co-localization of foreign fragments. A notable difference between the two approaches is that the proteins in the TMV system are expressed in the same cell, whereas in the oil body system, the proteins are expressed in different cells.

A number of foreign viruses have been used to express the oilseed crop protein. These include the turnip yellow leaf curl virus (TylMV) (Liu et al. 1992; Li et al. 1993), Trichoplusia ni baculovirus (BaculoV) (Liu et al. 1993), and TMV (Chen et al. 1993). Recombinant proteins were introduced with infectious RNA or DNA into plant cells carrying the foreign protein. Subsequent to the introduction of the recombinant protein, the cells are harvested from the infected plant material and harvested. While in this example, the purified recombinant protein is harvested for use in oil bodies, it is also feasible to purify further, purely recombinant proteins with this approach by introducing a protease cleavage site into the fusion protein. One possible advantage to this approach may be the size of the foreign protein, as larger proteins may impair viral coat assembly.

Secretion into the extracellular media or periplasmic space has proven to be extremely useful for production and purification of foreign proteins in many yeast and bacterial systems. In addition to providing an enhanced function of the recombinant product, secretion has also been found to enhance protein stability and facilitate proper folding. Another attractive feature of this approach is that the signal peptide is removed from the recombinant protein in the course of normal processing, enabling a authentic protein to be obtained without introducing additional proteolytic digestion steps. In plant cells, secreted proteins are deposited into the apoplastic space. The native signal peptide as well as a signal sequence

from the tobacco pathogenesis-related protein, PR-5, have been used to successfully direct expression of human serum albumin in potato (Sunami et al. 1990). Similarly, the plant protease inhibitor II protein signal peptide (Hirashima et al. 1995) has been used to provide cleavage into the apoplastic space of tobacco PR-5. The hydrolytic structure of the recombinant protein can be altered with this approach, making it a potentially effective means from the standpoint of both cost and safety.

With the aforementioned formats of fusion, it is also possible to target protein to the lumen of the ER or nucleus. The tobacco deetiolated leaf olatephelin has been expressed in seeds of *Arabidopsis thaliana*, *Brassica napus* and *B. juncea* as an intact fusion. Between the N- and C-terminal ends of the Arabidopsis 2S albumin protein (Nunes-Silva et al. 1989), the Olatephelin domain was subsequently found to be accountable solely within the protein bodies of these seeds. Purification was accomplished through differential fractionation in low salt to obtain albumin proteins followed by low molecular weight steps and HPLC separation. One drawback of this strategy is the complexity of the proteolytic cleavage, particularly since zeta-2案子 is required to process the C-terminal portion of the albumin protein. A failure to correctly cleave this region would result in significant protein heterogeneity. It is also possible by fusing domains for proteins both downstream and upstream of the lumen of the foreign protein that could be produced as an intact fusion.

Seed oil bodies represent another subcellular compartment utilized for storage of recombinant proteins. Addition of oil bodies is achieved through cryogenic fixation of seeds. In contrast to membrane proteins and globular proteins, recombinant proteins are distributed below oil bodies often only accidentally. In order to facilitate detection, separation, and purification of recombinant proteins, oil bodies must be disrupted prior to separation and purification of foreign proteins.

2.5.3. Seed Oil Bodies as Purification Tools

Oil bodies are natural subcellular organelles found in all seeds where they form the basis of 50% of the phytomycte energy reserves in these seeds (Boggs-Green et al. 1992). They are composed of TAG surrounded by a half-synthetically synthesized membrane into which is embedded a unique type of protein known as oleosin. Oleosins account for 2% to 10% of oil seeds comprising between 2% and 10% of the total seed protein in different species. It is believed that the primary function of oleosins is to prevent the coalescence of oil bodies during seed dehydration. In so doing, a larger surface area is available for lyophilic enzymes enabling the rapid mobilization of TAG reserves upon seed germination. Although the precise mechanisms of oleosin targeting is not fully understood, it is known that they are synthesized on the ER and that a motif in the central domain is crucial for their subsequent localization to oil bodies (Van Rossum and Moeser 1995; Asai et al. 1997). The oleosin protein appears to consist of three distinct domains. The N- and C-terminal domains are amphiphilic and proteolytic digestion studies strongly suggest that they reside on the outer surface of the oil body (Asai et al.

1997; Hill et al. 1993; Tzivs and Flavine 1992). The central domain is comprised largely of hydrophobic amino acid residues, and is believed to adopt a helix conformation anchoring the protein firmly within the TAG core of the oil body. Comparison of OilBody sequences from different species reveal that the central domain is highly conserved, while the N- and C-terminal exhibit considerable sequence variation.

Several features of oil bodies lend themselves to the production of oil bodies. OilBodies segregate large fractions of foreign proteins to either the N- or C-terminal ends without apparent loss of oil body targeting efficiency (Matsushige and VAN RODEN 1996). OilBodies function have been correlated with a number of different problems involving unanticipated weight gain of oil bodies, all of which are usually accompanied on the surface of oil bodies. In the case of this reported enzyme deficiency, it was further shown that enzymatic activity was maintained with the change in position of body envelope. The oil bodies, together with their complement of oil body proteins, are removed by simple bath washing the seed and following their removal by centrifugation (van Rooden and Lampeau 1995b). Without the seed, the proteins remain undegraded for years without the requirement for elaborate storage conditions. Following deseeding into aqueous solution, oil bodies are efficiently released by mechanical disruption and are stable over 10 days at pH and temperature (Aebischer et al. 1996; van Rooden and Moloney 1995b). Finally, the lower density of oil bodies allows them to be separated from soluble contaminants by flotation centrifugation, enabling simple and rapid purification of recombinant protein targeted to the oil body surface. Digestion with a site-specific protease to cleave the oleosin fusion protein, and centrifugation to remove the oil bodies, results in the recovery of a highly enriched fraction of the desired recombinant protein within the aqueous phase. The naturally low hydrolytic environment within the seed, coupled with the rapid removal of soluble-protein contaminants, ensure that little or no degradation of the oil body-associated proteins occurs during processing. As described in Sect 3.2, the unique properties of oleosins and oil bodies have been exploited by San BiSys in the development of a novel plant-based protein production and purification system.

3.1 Production of Human Lysosomal Enzymes in *Nicotiana tabacum*

Constitutive expression of recombinant lysosomal protein for replacement therapy is likely to have a huge impact on the care and treatment of patients with specific metabolic diseases (Table 1). Translational sports of disorders represent a large class of these genetic diseases for which the molecular basis of disease has been determined. Lysosomal enzymes encoding the required enzymes have been cloned (Napier 1991). However, the cellular specificity responsible for the regulated translocation of enzymes for intercellular location, contain multiple hydrophobic anchoring proteins (molecules, glycosidases, IgGs, phosphatases, phosphodiesterases, and sulfatases) (Korn et al. 1986). Deficiencies in specific lysosomal hydrolases can lead to toxic accumulation of the undigested substrate and a variety of clinical manifestations. Tay-Sach's Disease is perhaps the most familiar lysosomal storage disease, targeting neurons. It is characterized by the build up of gangliosides that lead to accumulation of ganglioside GM2 in the membranes of brain cells (Quaranta 1990). The main coproduct of Tay-Sach's disease is GM2. A group of neuronal storage diseases caused by deficiencies of one or more of the six lysosomal enzymes required for the degradation of sulfatidyl glycosphingolipids (reviewed in Nichols and Murraca 1993). Lysosomal accumulation of undegraded glycosphingolipids leads to the malfunction of affected cell organelles which compromises the growth and development of the individual and, in severe cases, lead to premature death. Replacement enzyme therapy appears promising based on human cell- and animal models, but drug development is hampered by the small patient pool and limitation in current technologies for cost-effective bioproduction. The industry paradigm for human replacement enzyme therapy is the glycoprotein product Cerezyme (Genzyme, Cambridge, MA) for the treatment of Gaucher disease. This lysosomal storage disorder affects 10,000–20,000 individuals in the United States (NTI Therapeutic Assessment Panel on Gaucher Disease 1996) and is caused by defect in glucuronidase, an acid β-glucuronidase required for complex lipid degradation. Routine administration (generally every 2 weeks) of plasma-derived enzyme has revolutionized the treatment of the disease and the quality of life of Gaucher patients. However, the high drug costs associated with production of therapeutic enzymes from human donors in a 200 mg weekly dose, and limitations of its availability, limit its use.

In addition to Cerezyme, many other glycoproteins are produced by pharmaceutical companies. The enzyme methods used and the potential for Orphan Drug status to facilitate products toward clinical trials and commercialization are discussed. Among these, the first glycoprotein enzyme produced in transgenic plants was glucuronyltransferase (GlcUT) (Cai et al. 1996a,b). Presented is a unique therapeutic strategy that has been entirely modified to generate mannosidase-terminated glycan. Its highly effective in-

3.2 Examples of protein-synthesized Protein Therapeutics Upstream and Downstream Strategies

In order to "apply to practice" many of the considerations and strategies described above, two very different examples of plant-based biopharmaceuticals to combat human health problems are described below. These examples set only demonstrate the diversity of expression and purification strategies available through plants, but also highlight the constraints on bioproduction strategies imposed by the natural properties of plants. In both cases, the overall bioproduction strategy has been strongly influenced by commercial and regulatory considerations.

present on the placental enzyme are histidine structures having terminal basic acid residues. In order to direct effective delivery to lysosomes of the affected cells in Gaucher patients (primarily cells of the macrophage/motocyte lineage), sequential enzymatic digestion is used to remove the terminal sugars and expose the mannose group (Maroff et al. 1991). This mannose-enriched form is targeted to the correct cell and organelle location to effect breakdown, degradation, and symptom resolution (Ghochikyan et al. 1991; Barron et al. 1991). Gaucher's disease symptoms are usually manifest or terminated (Chapman and Fawcett 1996; Enzymatic removal of the immunogenic fucose and galactose residues should yield glycoforms of amilase that are indistinguishable as a disease.

3.2 Production of Hirudin in *Bacillus subtilis*

To evaluate the potential of *Saccharomyces cerevisiae* partitioning technology, the model thrombin-binding protein Hirudin was selected. Hirudin is a naturally occurring anticoagulant protein produced in the salivary glands of bloodsucking leeches (*Hirudo medicinalis*) and secreted to facilitate feeding. Since its discovery almost 50 years ago, it has been extensively studied. Hirudin possesses a number of desirable properties which advocate its use as a therapeutic pharmaceutical. It is an entirely specific and potent inhibitor of thrombin, the last enzyme in the blood coagulation cascade, having a K_i of 2 nM (Blaauw et al. 1988). It is also rapidly cleared from the body, exhibiting low toxicity (500,000 U/kg body weight in rats) (Mavasany et al. 1982) and, probably as consequence of its cytological of leeches and mammals, has relatively low immunogenicity (Kloetzing 1991). The protein has also been well characterized with respect to its structure and mechanism of binding to thrombin (Gysel et al. 1990). A small number of closely related isoforms of Hirudin have been isolated all of which show high conservation for six cysteine residues (Soroush and Markowicz 1993). These residues participate in the formation of three disulfide bridges whose precise linking is necessary for protein activity (Gharabagi and Chano 1992, 1993). Although the native protein is purified at the 70-75% position, recombinant hirudin protein exhibits significant activity (Soroush and Markowicz 1993). It folds spontaneously *in vivo* and functional Hirudin has been produced previously in both bacterial (Hawley et al. 1995; Basner et al. 1990) and yeast (Zoson et al. 1991; Laiou et al. 1992) systems. However, the quantities of Hirudin required, were it to fully replace presently used anticoagulants such as heparin, are estimated to be on the order of hundreds to thousands of kilograms of protein annually. For this reason, Hirudin is an excellent candidate for production with a high capacity plant-based system.

The common oleaginous rape species *Brassica napus*, was selected as the vehicle for production of seed-derived Hirudin. After tobacco, the *Branntica* species are among those most easily transformed with Agrobacterium. Cells in the cotyledons of embryogenic protoplasts cul from young seedlings are readily infected with the bacterium. Formation of callus regeneration, and induction of transformation are all very efficient. In a recent transformation, efficiencies approaching 55% were obtained.

the original explants can be obtained. The time-line for development of a transgenic plant is also relatively short, in the range of approximately 4–6 months from transformation to collection of first generation transformed seed. Another attractive feature is the availability of a diploid production system from interspecific derived embryos, facilitating the creation of homogeneous lines. At an altered level, could a diploid be concentrated within the seed. Seed production in *B. rapae* is between 1 and 2 tons per hectare at a cost of approximately (United States) \$100/ton. Hirudin content in these seeds represents in excess of 20% of the total seed weight, approximately 5% of which is oleic acid.

The production and analysis of transgenic plants expressing an oleic acid/hindin fusion has been reported previously (Patterson et al. 1995). Briefly, a synthetic sequence encoding the Hirudin variant 2 (HV2) domain was fused to the 3' end of an *Arabidopsis* 12 kDa oleic acid gene with the two coding regions separated by a sequence encoding the foreign oil acid recognition site for the proteinase, *Xanthoxylon*. Following *Agrobacterium*-mediated transformation, putative transgenic lines were selected and expression of the oleic acid/Hirudin fusion confirmed by Northern analysis. Immunoblotting with anti-Hirudin antibodies demonstrated that the oleic acid-Hirudin fusion protein was correctly expressed and accumulated on oil bodies of Arabidopsis seed. Oil bodies were separated and washed to remove contaminating oil bodies through flotation-centrifugation. After digestion with factor Xa and a final round of flotation-centrifugation to remove oil bodies, Hirudin was recovered in the aqueous fraction. Formation of a functional protein was confirmed by an *in vitro* thrombin inhibition assay. Comparison of Purified oleic acid/Hirudin extract and in the soluble fraction obtained after flotation centrifugation indicated that the majority of seed protein had been removed. The experiment obtained with this procedure demonstrated the utility of oil body compartmentalization for purification of recombinant proteins. Further purification of the recombinant Hirudin to near homogeneity was achieved through anion exchange and reverse phase chromatography. Values obtained for the specific activity of *B. rapae*-derived Hirudin (Linson et al. 1988).

3.3 Prospects of OleoPro-Partitioning Technology

The potential for commercial application of oleoPro partitioning technology can be evaluated by examining the system with reference to certain key production parameters namely, production capacity, authenticity/insurability of product, downstream purification costs, and process scalability. We have estimated the level of expression of the oleic acid-Hirudin fusion protein in our transgenic seed to be approximately 10% of that of the endogenous oleostearin (Patterson et al. 1995). Based on this estimate, hirudin would represent approximately 0.3% of the total seed protein. While reengineering, this level is still somewhat lower than would be desired for a commercial production system. To increase expression levels, we are currently testing a number of strong seed-specific promoters other than those in our fusion construct. An increase in the expression of recombinant protein to the relatively

modest level of 1% of seed protein would result in a system capacity of approximately 2kg of product per ton of seed. When coupled with low production costs and cost-effective purification, this level is within the range required for commercial viability.

The downstream purification of proteins synthesized by oleosin fractions is greatly simplified by the oil body separation process. However, in order to do this process to be cost-effective, the fusion protein cleavage step must be both efficient and economical. While useful for demonstration purposes, the factor 2A used in our initial feasibility studies fails to meet these requirements. The enzyme is expensive, gave incomplete cleavage, and represented a contaminant which had to be removed in subsequent purification steps. To address this problem, we are presently expressing protease subunit fusion proteins immobilized on the surface of oil bodies. This will enable both economical production of the protease and easy removal following fusion protein cleavage through the existing oil body separation process. A number of suitable candidate proteins have been identified and are currently being tested.

The importance of process scale-up in determining economic feasibility is often overlooked in the initial research and developmental phase of a new biotechnology. Procedures that work well for typical laboratory-scale experiments cannot always be directly scaled up or easily adapted to existing industrial processes. In the case of oleosin partitioning technology, we have developed and tested methods using industrial equipment for the large scale preparation of oil bodies. The results from these tests indicate that the process can be easily scaled up to meet commercial production requirements.

The recovery of some products such as arabin and D-mannose from oleosin fusion demonstrates that functional proteins can be produced using oleosin partitioning technology. However, the fact that oleosins are not exposed to the lysate of the ER under normal conditions has raised concern regarding the use of these oil bodies in other forms of downstream processing. Modification of the oil bodies through the endoplasmic reticulum would not be prominently perceived as a serious concern. However, further downstream modification would be desired through the endoplasmic reticulum. This technology is well amenable to production using this technology. In addition to those results mentioned, the oil bodies play food and industrial compounds. Some of these products are differently under development. Additionally, the ability to produce functional proteins on the surface of oil bodies offers exciting new possibilities for the production of claim-protected pharmaceuticals. As shown by Chappel et al. (1993), high quality recombinant proteins can be produced using this technology. In light of the areas mentioned above, prospects for the successful commercialization of oleosin partitioning technology appear very promising.

4 Summary

We have described two very different and innovative plant-based production systems - postharvest production and recovery of recombinant product from tobacco

lines using an inducible promoter and oleosin-mediated recovery of recombinant products from oleosins using a seed-specific promoter. Both base technologies are broadly applicable to numerous classes of pharmaceutical and industrial proteins. As with any engineering technology, the key to success may lie in identifying those products and applications that would most benefit from the unique advantages offered by each system. The postharvest tobacco leaf system appears effective for proteins requiring complex posttranslational processing and endogenous targeting. Because of its remarkable locality and bypasses represent significant benefits of tobacco, biomass scalability is very rapid and production costs are low. Clearly, the development of equally cost-effective extraction and purification technologies will be critical for full realization of the potential opportunities afforded by transgenic plant-based bioproduction. The recovery of protein from tobacco leaves or oleosin partitioned proteins by high separation represent significant breakthroughs for cost-effective commercialization strategies. Additional烟草中高亲和力分离技术需要开发以实现有效的大规模生产。显然，通过植物表达的生物活性蛋白的纯化技术将对实现该潜力至关重要。从烟草中回收蛋白或通过油体分离表达蛋白，这两种方法都展示了巨大的优势。然而，要实现大规模生产，仍需进一步优化纯化技术。

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directive challenge for production in plants as well as other recombinant expressed systems (Trommsdorff et al. 1993). For soluble lysosomal enzymes such as IDUA, the signal for lysosomal sorting is the mannose-6-phosphate residues present in their N-linked glycans. Mannose-6-phosphate recognition sites are present on the lysosomotropic enzymes as well as lysosomal membrane proteins of many mammalian cell types and thus direct uptake and lysosomal delivery of exogenously supplied IDUA (Kuroki et al. 1996). Plants do not phosphorylate their glycans and glycan-based signals do not appear to function in vacuolar targeting (Ravex et al. 1988; Genschens and Faverot 1998). It is likely that some, if not all, of the glycans on tobacco-synthesized IDUA are in the complex form and thus likely to be immunogenic (see Sect. 2.4) and ineffective in directing the required cell-specificity for uptake and lysosomal delivery. Engineering plants to synthesize mannose-6-phosphate-modified glycans is currently not feasible – the two required enzymes have not been well characterized. However, alternative strategies that address both the delivery and immunogenicity are suggested by the currently effective lysosomal replacement therapeutic, Cerezyme. Glucocerebrosidase is a membrane-associated protein that is targeted to lysosomes by a mannose-6-phosphate-independent route. The N-linked glycans

of IDUA synthesis in human mucopolysaccharidosis type II (MPSII) fibroblasts were described. Furthermore, a 24-hr culture supernatant from MPSII fibroblasts contained a protein which inhibited IDUA activity in rat liver homogenates. This inhibitor was found to be a glycoprotein with a molecular weight of 100,000 daltons. The inhibitor was found to bind to the IDUA enzyme, and it was suggested that the inhibitor may be a normal component of the human mucopolysaccharide complex. The inhibitor was also found to inhibit IDUA activity in rat liver homogenates, and it was suggested that the inhibitor may be a normal component of the human mucopolysaccharide complex.

dusion of glucocerebrosidase (*Ceradase*, Genzyme), it requires between 400 and 2000 phosducine to supply a standard dose – a major factor in the extreme cost to

of 653 amino acids (pre-IDUα) with a signal peptide cleavage site at amino acid 27. The cDNA for IDUA has been expressed in COS-1 and CHO cells (KAMIKOSHIKA et al., 1994; SOOFT et al., 1991) and recombinant IDUA has been purified and shown